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AIR QUALITY PERMIT TO CONSTRUCT APPLICATION  
MODELING PROTOCOL  
Commercial Fuel Recycling, LLC  
720 N. Sugar Street  
Nampa, Idaho 83687

Department of Environmental Quality  
State Air Program

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October 31, 2007

Prepared for: Commercial Fuel Recycling, LLC  
3116 Garrity Boulevard  
No.7, PMB #63  
Nampa, Idaho 83687

For the Facility at: 720 N. Sugar Street  
Nampa, Idaho 83687

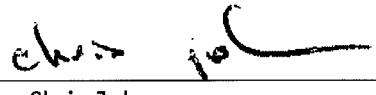
Prepared by: TORF Environmental Management  
3459 E. Boulder Heights Drive  
Boise, Idaho 83712

(208) 571-2393  
(208) 345-8285 FAX  
[www.torf.us](http://www.torf.us)

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Sarah L. Stine, P.E.  
Sr. Engineer

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Chris Johnson  
Meteorologist

**AIR QUALITY PERMIT TO CONSTRUCT APPLICATION  
MODELING PROTOCOL**  
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720 N. Sugar Street  
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## 1.0 PROJECT DESCRIPTION AND PURPOSE OF MODELING

Commercial Fuel Recycling, LLC (Commercial Fuel) proposes to obtain an Air Quality Permit to Construct (PTC) for a used oil recycling facility at 720 N. Sugar Street in Nampa, Idaho. The plant is located in an industrial area, between Garrity Boulevard and Interstate 84, in northeast Nampa. UTM coordinates at the site are 537,004 meters (X, Easting) and 4,826,309 m (Y, Northing).

This modeling protocol is a follow up to an earlier protocol submitted for the same facility on July 11, 2007. The primary changes in the current protocol are that the proposed permitted facility throughput was increased from 3.0 to 3.5 MM gallons/year of used oil, and that air dispersion modeling was accomplished with AERMOD rather than SCREEN3. The methodology used to qualifying and quantifying process streams and emissions is unchanged.

The facility is applying to receive a PTC as a minor source of air pollutant emissions. Emission sources at the facility include a natural gas-fired boiler, three (3) product storage tanks, and four (4) oil processing tanks. Emissions include criteria pollutants, hazardous air pollutants (HAPs), and toxic air pollutants (TAPs) associated with natural gas combustion and the heating and handling of used oil. In 2006, the facility processed 2,070,000 gallons of used oil. The previous years' amounts were less.

A facility plot plan is provided in Figure 1 (attached). Three of the tanks on the site are vertical, cylindrical tanks ranging in volume from 60,000-150,000 gallons. These tanks (#1-3) are used for storage of the processed oil. Four of the tanks on site are horizontal, cylindrical tanks ranging in volume from 10,000-13,000 gallons. These tanks (#5-8) are used for short-term storage and processing of the used oil feed. The recycling process involves heating a tank of oil to approximately 220°F to remove water, while simultaneously circulating the oil through a series of filters to remove particulate contaminants. Processing time is typically 16-24 hours.

A glycol-water mixture is circulated through heating coils in the processing tanks to heat the used oil. The glycol solution is heated to approximately 320°F in a Parker Model T-6800 Hot Water Boiler with a design duty of 6.8 MMBtu/hr. The boiler fuel is natural gas.

## 2.0 DESCRIPTION OF EMISSIONS QUANTITIES

Emissions from the combustion of natural gas in the Parker boiler are calculated in Tables 1-a (criteria) and 1-b (TAPs), attached. Emission factors from AP-42, Chapter 1.4 were used to estimate emissions at the design input duty of 6.8 MMBtu/hr.

Emissions from the storage and processing tanks are associated with "breathing" losses- vaporization caused as ambient conditions change- and "working" losses- vapor emissions caused when the tank levels change. In addition, processing tank emissions are also caused when the oil is heated to 220°F and water and hydrocarbons are vaporized.

Tank emissions were estimated using the U.S. Environmental Protection Agency's (EPA's) TANKS software, Version 4.0.9d. The TANKS software allows users to input specific location, size, configuration, and content data. The location for all the tanks was input as Boise- the closest option offered by the program.

#### Product Storage Tanks 1-3

TANKS Run Reports for the three vertical storage tanks, Tanks 1-3, are provided in Appendix A and summarized in Table 2, attached. Emissions are estimated assuming a controlled throughput of 3.5 MM gallon per year, the proposed permit limit. The 3.5 MM gal/yr throughput is assumed to be distributed evenly among Tanks 1-3 in proportion to their relative sizes. The average liquid height in each tank is assumed to be 50%. TANKS calculations to estimate "uncontrolled" emissions from Tanks 1-3 were not done since uncontrolled emission estimates from Tanks 5-8 indicate that facility throughput must be controlled to meet air quality standards (see discussion below).

The Recycled Fuel Oil Product (RFOP) stored in Tanks 1-3 is characterized using a combination of analytical data and embedded TANKS options. A sample of RFOP was analyzed using EPA Methods 8260 and 8270. These results are provided in Appendix B. The specific hydrocarbon compounds detected, which total less than 0.2 wt%, are entered into TANKS. The remainder of the contents is specified as Residual Oil No. 6, a TANKS option.

#### Used Oil Processing Tanks 5-8

TANKS Run Reports for the four horizontal tanks, Tanks 5-8, are provided in Appendix A. The TANKS program is set up to estimate monthly and annual emissions. In order to conservatively estimate the working and heating losses associated with processing each batch of oil, Tanks 5-8 are assumed to be processing a full tank of oil each day. The resulting annual emissions can be considered "uncontrolled" emissions as defined in IDAPA 58.01.01.210.b, since processing one batch of oil per day in each tank would be the most the facility is capable of.

The used oil processed in Tanks 5-8 is characterized using a combination of analytical data and embedded TANKS options. A sample of used oil was analyzed using EPA Methods 8260 and 8270. These results are provided in Appendix B. The specific hydrocarbon compounds detected, which total less than 0.2 wt%, are entered into TANKS. The remainder of the contents is specified as Residual Oil No. 6, a TANKS option. The default TANKS option for Residual Oil No. 6 limits accurate vapor pressure calculations to 100°F. To allow TANKS to accurately calculate emissions at the processing temperature of 220°F, Antoine's constants (A=83,897.34, B=9.503) were entered.

The uncontrolled emissions from Tanks 5-8 are summarized in Table 3, attached. Operations with all four processing tanks in this manner result in an uncontrolled facility annual throughput of 14.8 MM gallons per year. As shown in Table 3, emission levels of benzene are above the IDAPA 58.01.01.586 Toxic Air Pollutant screening emission level. Screening emissions analyses (see

07/11/07 Modeling Protocol) indicated that the uncontrolled ambient air benzene concentration is above the acceptable level of 0.12 ug/m<sup>3</sup> (IDAPA 58.01.01.586). Therefore, "controlled" emissions from operations at a proposed permitted annual throughput of 3.5 MM gallons per year are estimated.

Dividing the estimated uncontrolled emissions from each process tank by 365 days allows the per batch emissions from each tank to be estimated. To estimate controlled annual emissions, each tank's annual throughput is determined by dividing 3.5 MM gal/year between Tanks 5, 6, 7, and 8 in a 40/40/10/10% split. Tanks 5 and 6 are insulated and are used most often as the processing tanks. Heating capability was recently added to Tanks 7 and 8, and they are also used as processing tanks, though less frequently because they are not insulated.

Each processing tank's controlled annual throughput is divided by their respective working volume to determine the annual number of batches. Estimated controlled emissions from each tank are then calculated by multiplying the number of batches by the per batch emission rate established above. The results are shown in Table 3.

A facility-wide controlled emissions summary incorporating the proposed throughput limit and unrestricted boiler emissions is provided in Table 4, attached.

### 3.0 MODELING APPLICABILITY ASSESSMENT

#### 3.1 Criteria Pollutant Modeling Applicability

Nitrogen oxides (NO<sub>x</sub>) are the only criteria pollutants with emissions above IDEQ modeling thresholds and, therefore, the only criteria pollutant modeled. The CO, lead, PM<sub>10</sub>, and SO<sub>2</sub> emissions from the boiler do not exceed the IDEQ modeling thresholds and, therefore, are not included in air dispersion modeling (see Table 1-a). There are no other known process sources of CO, lead, PM<sub>10</sub>, and SO<sub>2</sub> emissions.

#### 3.2 TAPs Modeling Applicability

The uncontrolled emission rates of all TAPs except benzene and cadmium and are less than the emission screening levels listed in IDAPA 58.01.01.585 (see Tables 1-b, 2, and 3). According to Permit to Construct regulations provided in IDAPA 58.01.01.210.05, these TAPs do not require further analysis. The controlled emissions of benzene and cadmium were analyzed to demonstrate that the controlled ambient concentrations are less than the acceptable ambient concentrations for carcinogens (AACCs), in accordance with IDAPA 58.01.01.210.08.

### 4.0 MODELING ANALYSES METHODOLOGY

#### 4.1 Model Used

Consistent with IDEQ's recommendations in the 08/06/07 *Modeling Protocol Approval Letter*, the model chosen was AERMOD, the United States Environmental Protection Agency (USEPA)-approved

dispersion model. AERMOD, one of the most frequently used regulatory dispersion models in the United States since it replaced ISCST3 in EPA guidance, is the most appropriate of the EPA-approved models given the site's physical characteristics and the variety of facility emission sources.

The sophisticated Prime building downwash algorithm was conservatively applied for the facility. The model was applied as recommended in EPA's Guideline on Air Quality Models (2001), utilizing that document's regulatory default options and the simple and complex terrain options and other input settings consistent with State of Idaho Air Quality Modeling Guideline. The modeling of the tank vents with stacks reflecting actual release scenarios is consistent with recommendations by Darrin Mehr (*08/06/07 Modeling Protocol Approval Letter*).

#### 4.2 Criteria Pollutant Modeling Methodology

The facility emission inventory verified one criteria pollutant with the potential to be emitted above IDEQ modeling threshold: NO<sub>x</sub>. The facility is applying for its initial air quality permit so the NO<sub>x</sub> is modeled as part of a Full Impact Analysis. All facility NO<sub>x</sub> emissions are modeled, not just increases from any prior period. NO<sub>x</sub> has an IDEQ ambient impact limit for the annual average period only.

The result of an AERMOD air dispersion analysis of NO<sub>x</sub> impact using the unrestricted emission rate from the boiler is shown in Table 6 (see Section 6). Model inputs are discussed in Section 5, below. Model results reported are the maximum annual average impact at any model receptor in any of the five years modeled. IDEQ supplied a NO<sub>x</sub> background concentration of 32 ug/m<sup>3</sup> to account for existing NO<sub>x</sub> in the Nampa area (*08/06/07 Modeling Protocol Approval Letter*).

#### 4.3 TAPs Modeling Methodology

The facility emission inventory verified two TAPs with the potential to be emitted above IDEQ modeling thresholds: benzene and cadmium. The facility is applying for its initial air quality permit so the TAPs are modeled as part of a Full Impact Analysis. All facility TAP emissions are modeled, not just increases from any prior period. Benzene and cadmium have IDEQ ambient impact limits for the annual average period only.

Facility-wide controlled TAP emissions are summarized in Table 4 based on the proposed permit facility throughput limit and include the estimated uncontrolled boiler emissions. The results of an AERMOD air dispersion analysis of benzene and cadmium impacts are shown in Table 6 (see Section 6). Model inputs are discussed in Section 5, below. Model results reported are the maximum annual average impact at any model receptor in any of the five years modeled.

## 5.0 MODEL INPUT DATA

### 5.1 Meteorological Data, Receptor Network

Five years of National Weather Service data from the Boise airport, from 1988 to 1992, are used. The meteorological data are in a single, five-year file prepared and provided by IDEQ, who recommended it for this application.

The model includes rural and urban algorithm options. These options affect the wind speed profile, dispersion rates, and mixing-height formula used in calculating ground-level pollutant concentrations. A protocol was developed by USEPA to classify an area as either rural or urban for dispersion modeling purposes. The classification is based on average heat flux, land use, or population density within a three-km radius from the plant site. Of these techniques, the USEPA has specified that land use is the most definitive criterion (USEPA, 1987). The urban/rural classification scheme based on land use is as follows:

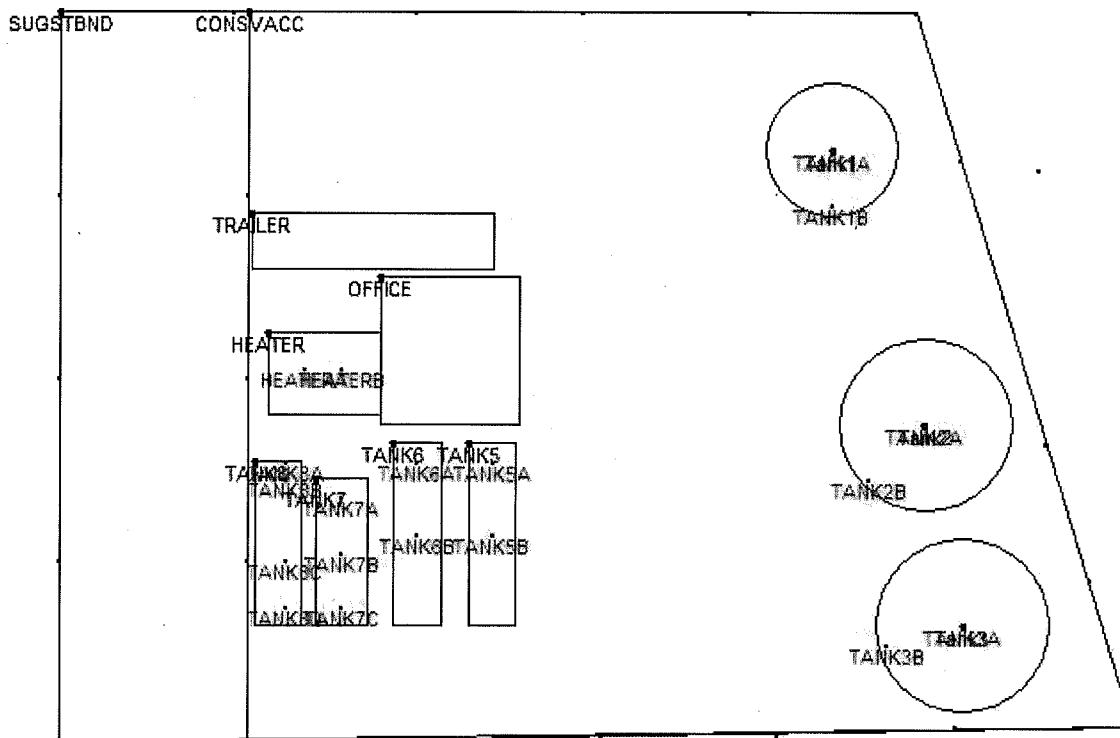
*The land use within the total area,  $A_0$ , circumscribed by a 3-km circle about the source, is classified using the meteorological land use typing scheme proposed by Auer (1978). The classification scheme requires that more than 50% of the area,  $A_0$ , be from the following land use types in order to be considered urban for dispersion modeling purposes: heavy industrial (I1); light-moderate industrial (I2); commercial (C1); single-family compact residential (R2); and multi-family compact residential (R3). Otherwise, the use of rural dispersion coefficients is appropriate.*

The Commercial Fuels facility is located in an industrial area on the northeast side of Nampa. The majority of the three kilometer circle would include low-rise industrial and residential land uses, with few structures sufficiently high to cause urban wind channeling. Rural dispersion coefficients are therefore used in the air quality dispersion modeling.

Figure 2, below, shows the layout of the Commercial Fuel facility, and the model depiction of the sources and buildings within the facility, along with the facility boundary and inner fence line. Public access to most of the facility property is physically prevented by a 6-8' fence along the property boundary on the north, east and south sides, and immediately adjacent to Processing Tank 8 and the Heater Building on the west side. The property outside the fence to the west along Sugar Street is used for truck loading. Employees are trained to discourage or report unauthorized access in the truck loading area. The general public is not routinely invited onsite.

The fence line is used as the ambient access boundary. However, because public access is prevented from the rest of the property by trucks and/or staff, and because all analyses described are for annual average impacts, the property boundary could qualify as the ambient air boundary. Estimating ambient concentrations at the fence line is very conservative.

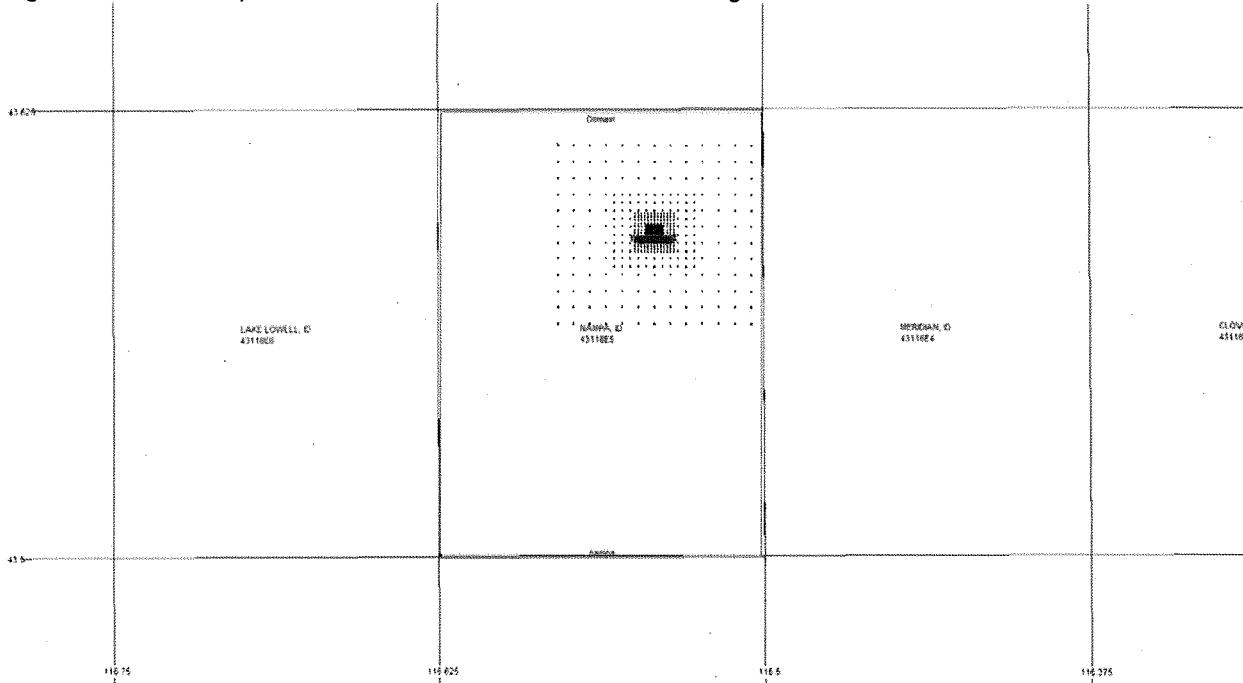
Figure 2: Emission Sources, Building, and Property Boundary / Public Access Limits



Facility emission sources are shown in red in Figure 2. The inner receptors are spaced 10 meters apart, inside the fence line. The dots along the fence line boundary represent the nearest model receptors. The model receptor network used in this analysis includes 10 meter grid spacing around the fence line, 25 meter grid density for the first 75 meters beyond, 50 meter grid density out to 200 meters, 100 meter grid spacing out to 600 meters, 250 meter grid density to 1200 meters, and 500 meter grid density to 2500 meters. All model predicted maximum impacts occur along the fence line in the area of 10 meter grid spacing.

The model domain is calculated by the BeeLine BEEST program to conservatively include the entire USGS quadrangle map (except for squared corners) covering any point with elevations meeting the AERMOD guidance requirements. In this analysis, that represented just one USGS quad map, because the area and its surroundings feature generally flat terrain. The AERMAP program is used to set elevations for all model buildings, source bases, and model receptors, and to process elevation and terrain data to be ready for the AERMOD analysis. Figure 3, below, shows the outer model receptor network, the model domain (outlined in green), and the corresponding USGS topographic map areas covered.

Figure 3: Outer Receptor Network, with Boundaries and Buildings



## 5.2 Emissions Release Parameters

Sources modeled include all emission sources documented in the emission inventory for all pollutants emitted above IDEQ modeling thresholds. The tank release vent data is presented as stacks, consistent with IDEQ recommendations. Actual stack data is used in the model for all heated tank and non-tank vent release sources. Stack data (height, orientation, presence of physical blockage, exhaust flow, and/or temperature) for all stacks were checked in the field by facility managers and/or TORF Environmental Management engineers.

All tank vent releases are modeled with actual release diameter or areas, and conservatively assumed to have minimal exit velocity of 0.001 m/sec. All onsite buildings and tanks are considered for downwash, using the Prime downwash algorithm. No fugitive sources of any of the pollutants (other than the tank releases IDEQ recommended be modeled as point sources) are identified or modeled.

Table 5, below, shows the model source parameters for all model sources and all pollutants modeled.

Table 5: Emission Release Data

POINT SOURCES		Easting (X) (m)	Northing (Y) (m)	Base Elevation (m)	Stack Height (ft)	Temp (°F)	Exit Velocity (m/s)	Stack Diameter (ft)	NOx (lb/hr)	Benzene (lb/hr)	Cadmium (lb/hr)
EP#	Source ID	Stack Type									
1	HEATERA	VERTICAL	536986	4826314	770.1	15.5	450	2.4	2.0	0.3130	7.00E-06
2	HEATERB	VERTICAL	536988	4826314	770.1	17.5	450	2.4	2.0	0.3130	7.00E-06
3	TANK1A	PCV	537014	4826326	770.9	25.25	53	0.001	0.67		4.53E-06
4	TANK1B	VERTICAL	537014	4826323	770.9	24.67	53	0.001	1.21		1.49E-05
5	TANK2A	PCV	537019	4826311	770.6	29.55	53	0.001	0.67		8.22E-06
6	TANK2B	VERTICAL	537016	4826308	770.6	28.63	53	0.001	1.33		3.29E-05
7	TANK3A	DOWNWARD	537021	4826300	770.6	23.90	53	0.001	0.25		9.69E-07
8	TANK3B	VERTICAL	537016	4826299	770.6	20.43	53	0.001	1.33		2.76E-05
9	TANK5A	RAINCAP	536996	4826309	770.0	13.92	140	0.001	2.00		1.47E-04
10	TANK5B	VERTICAL	536996	4826305	770.0	15.75	140	0.001	0.25		2.30E-06
11	TANK6A	RAINCAP	536992	4826309	770.0	13.92	140	0.001	2.00		1.47E-04
12	TANK6B	VERTICAL	536992	4826305	770.0	15.75	140	0.001	0.25		2.30E-06
13	TANK7A	VERTICAL	536988	4826307	770.0	14.4	140	0.001	1.58		1.20E-05
14	TANK7B	VERTICAL	536988	4826304	770.0	15.07	140	0.001	1.67		1.33E-05
15	TANK7C	VERTICAL	536988	4826301	770.0	14.4	140	0.001	1.58		1.20E-05
16	TANK8A	VERTICAL	536985	4826309	770.0	13.17	140	0.001	0.17		1.33E-07
17	TANK8B	VERTICAL	536985	4826308	770.0	13.00	140	0.001	1.58		1.20E-05
18	TANK8C	VERTICAL	536985	4826304	770.0	13.50	140	0.001	1.67		1.33E-05
19	TANK8D	VERTICAL	536985	4826301	770.0	13.00	140	0.001	1.58		1.20E-05

The heater exhausts through two side-by-side 24" stacks, centers six feet apart. Per the manufacturer, the exhaust flow rate is 3000 ACFM at 400-475°F. The 3000 ACFM exhaust flow rate is equivalent to an exit velocity of 8.0 ft/s (2.4 m/s) from each stack. The benzene, cadmium and NO<sub>x</sub> emissions calculated in Tables 1 and 2 are distributed evenly between the two stacks.

The emission release parameters for the three product and four processing tanks are also listed in Table 5. Based on Boise meteorological data, TANKS determined that the average annual temperature of Storage Tanks 1-3 is 53°F. This average is used as the emission temperature for the storage tanks. The temperature of Processing Tanks 5-8 varies between ambient and a maximum of 220°F. An average emission temperature of 140°F is used as the AERMOD input for the processing tanks.

The seven tanks are equipped with two to four emission openings each, ranging in diameter from 2 inches to 2 feet. Benzene emissions from each tank as estimated in Tables 2 and 3 are distributed between openings based on each opening's relative open area. This emission distribution is shown in Table 5.

### 5.3 Elevation Data

All elevation heights used in this modeling analysis are calculated from USGS NAD 27 7.5-degree (30m or less horizontal resolution) DEM data using the Bee-Line BEEST preprocessing system and the AERMAP program.

There are two permanent buildings at the facility, an office building and the boiler building (see Figure 1). The buildings' roofs are pitched. The office building roof is 17.4 feet high at its peak, while the boiler building's peak roof height is 13.75'. A single-wide trailer used for additional office space is located just to the north of the processing area. The trailer's height is 11.75' above grade.

Site and source elevations were determined by combining site topographical data with field-collected data on building, pad, tank, tank opening and stack heights. The area in and around the site is relatively flat, with gradual elevation changes. The base elevation and emission height of each emission source are listed in Table 5.

### 6.0 Evaluation of Compliance with Standards

Table 6, below, summarizes the results of the AERMOD air dispersion analysis for the site. The ambient air quality impact limits applicable to this analysis for criteria pollutants are the National Ambient Air Quality and identical IDAPA Standards for NO<sub>x</sub>, and the IDAPA 58.01.01.586 AACCs for the carcinogens benzene and cadmium. The maximum ambient concentration shown in Table 6 compared against the applicable impact limit is the maximum model-predicted impact at any receptor in any year. Background concentration is added to predicted maximum NO<sub>x</sub> impact to compare maximum operational NO<sub>x</sub> concentration against the NAAQS.

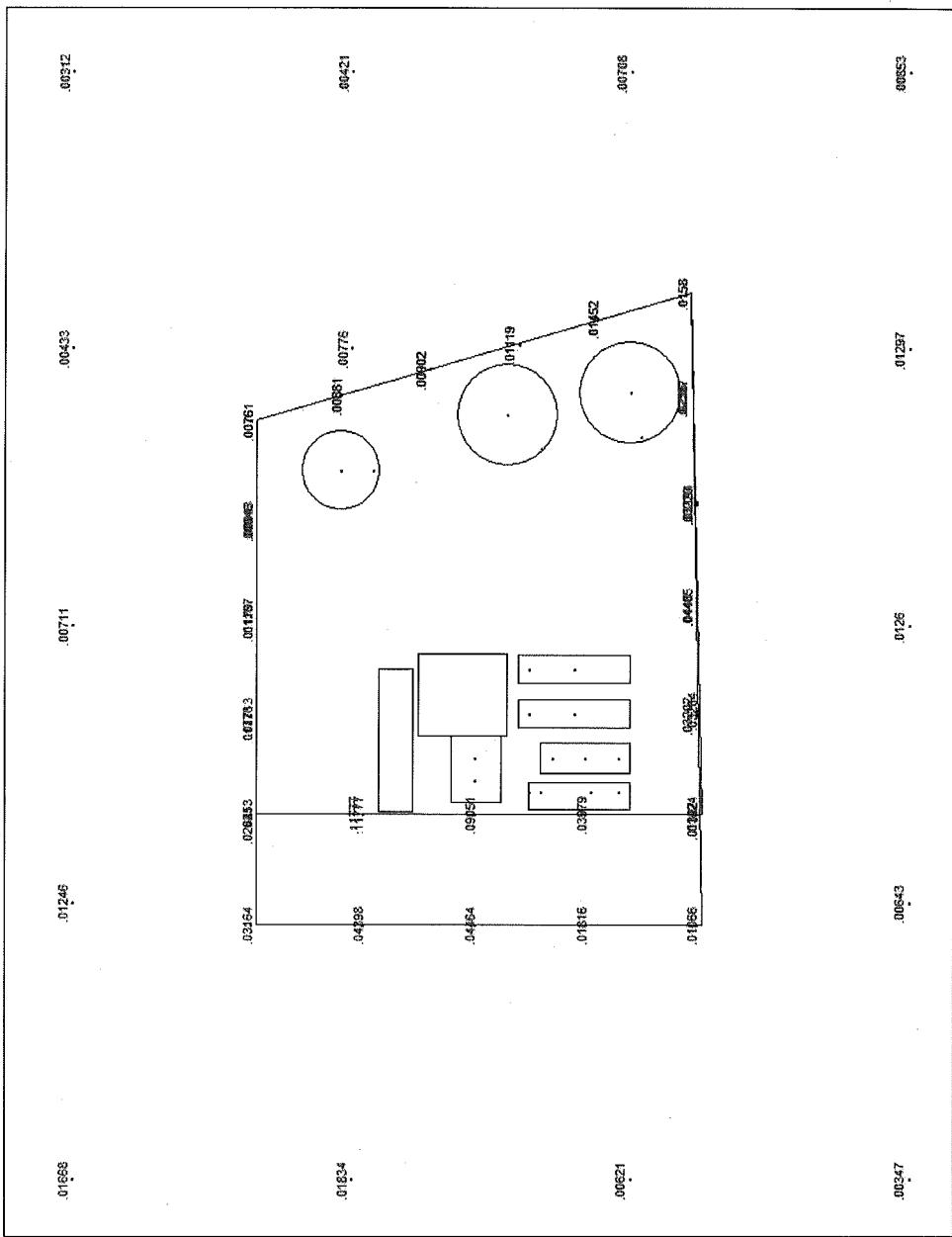
Table 6: Comparison of Predicted Impacts with Applicable Ambient Standards

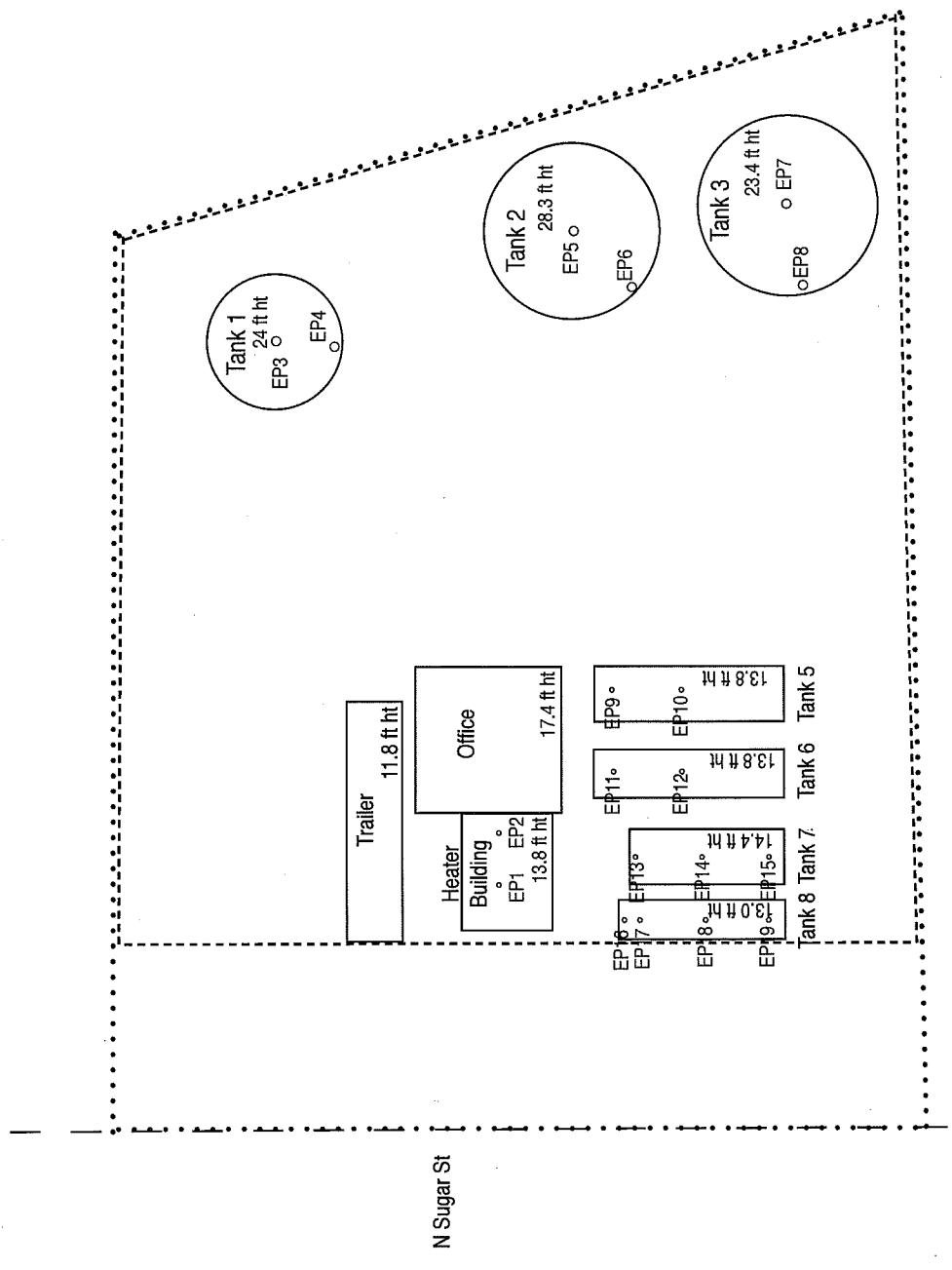
Pollutant	Averaging Period	Background Conc. ( $\mu\text{g}/\text{m}^3$ )	Modeled Worst Case Impact ( $\mu\text{g}/\text{m}^3$ )	Maximum Ambient Conc. ( $\mu\text{g}/\text{m}^3$ )	NAAQS or AACC ( $\mu\text{g}/\text{m}^3$ )	Location Of Highest Model Impact
NO <sub>x</sub>	Annual	32	18.7	50.7	100	S fence line
Benzene	Annual	-	0.118	-	0.12	W fence line NW of office
Cadmium	Annual	-	0.00021	-	0.00056	S fence line

Maximum predicted annual average impacts for all pollutants occur along the fence line. Only one pollutant, benzene, has maximum predicted impacts greater than 51% of allowable levels. Maximum benzene impacts along the west fence line are strongly influenced by building downwash, and drop off by an order of magnitude within 50 meters of the fence line. Figure 4, below, shows that maximum benzene impact at the western property boundary is 0.045  $\mu\text{g}/\text{m}^3$ , less than 40% of the AACC for benzene.

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**Commercial Fuel, Nampa, Idaho**  
**October 31, 2007**  
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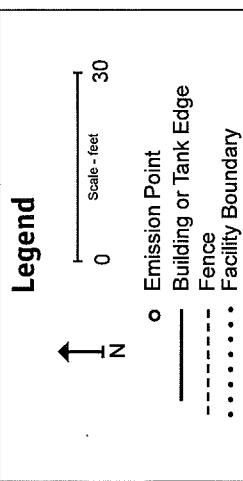
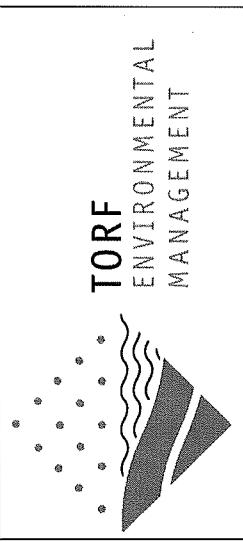
**Figure 4: Model-Predicted Benzene Annual Impacts**





**Figure 1: Plot Plan**  
**Commercial Fuel Recycling, LLC**  
**720 N Sugar Street**  
**Nampa, Idaho**

October 2007



**Table 1-a:**  
**Tank Heater Criteria Pollutant Emissions Analysis**

Natural Gas-Fired Equipment	Make	Rated Input (MMBtu/hr)	On-Line Rating hrs/yr	Fuel Rate <sup>1</sup> (scfh)	Emission Factors		Uncontrolled Emissions		Modeling Threshold					
						AP-42	Ib/MM scf	Ib/hr	tons/yr	Ib/hr	tons/yr			
Tank Heater	Parker	6.800	8760	6667	NO <sub>x</sub>	Table 1.4-1.	94	0.63	2.74	--	1.0			
					CO	Table 1.4-1.	40	0.27	1.17	14	--			
					SO <sub>2</sub>	Table 1.4-2.	0.6	0.0040	0.0175	0.2	1.0			
	T-6800				PM <sub>10</sub>	Table 1.4-2.	7.6	0.0507	0.2219	0.2	1.0			
					Lead	Table 1.4-2.	0.0005	3.33E-06	1.46E-05	--	0.6			
					VOC	Table 1.4-2.	5.5	0.0367	0.1606	--	--			

Note 1: Assume natural gas heating value of 1020 Btu/scf.

**Table 1-b:**  
**Tank Heater Toxic Air Pollutant Emissions Analysis**

Unit ID	Rated Input MMBtu per hr	On-line Rating Used (hrs/yr)	Emission Factor AP-42 Tables 1.4-3 and 1.4-4		Uncontrolled Combustion Emissions	58.01.01 Screening Level
			Toxic Air Pollutant	Ib/MMBtu		
<b>Tank Heater Parker T6800 HW Boiler</b>	6.800	8760	Arsenic	2.0E-07	1.3E-06	1.50E-06
			Barium	4.3E-06	2.9E-05	0.033
			Benzene	2.1E-06	1.40E-05	8.00E-04
			Cadmium	1.1E-06	7.3E-06	3.70E-06
			Chromium	1.4E-06	9.3E-06	0.033
			Cobalt	8.2E-08	5.6E-07	0.0070
			Copper	8.3E-07	5.7E-06	0.07
			Dichlorobenzene	1.2E-06	8.0E-06	20
			Formaldehyde	7.4E-05	5.0E-04	5.10E-04
			Hexane	1.8E-03	0.012	12
			Manganese	3.7E-07	2.5E-06	0.060
			Mercury	2.5E-07	1.7E-06	0.001
			Molybdenum	1.1E-06	7.3E-06	0.333
			Naphthalene	6.0E-07	4.1E-06	3.33
			Nickel	2.1E-06	1.4E-05	2.70E-05
			Pentane	2.5E-03	1.7E-02	118
			Toluene	3.3E-06	2.3E-05	25
			Vanadium	2.3E-06	1.5E-05	0.003
			Zinc	2.8E-05	1.9E-04	0.067

**Table 2:**  
**Storage Tanks 1-3 Estimated Emissions**

TANKS Input Data		Tank 1	Tank 2	Tank 3
Tank Type		Vertical, Fixed Roof, Unheated		
Roof Type		Flat		3' Ctr Pitch
Tank Contents		Recycled Fuel Oil Product		
Tank Exterior		Silver Paint (entered as "White")		
Tank Length (ft)		24.0	28.3	20.1
Tank Diameter (ft)		22.9	29.9	30.0
Tank Capacity (gals)		74,000	150,000	110,000
Tank Working Vol (gals)		60,000	135,000	100,000
Average Level		50%	50%	50%
Annual Throughput (gal/yr)	Total	3,500,000		
	Per Tank	711,864	1,601,695	1,186,441
Batches per Year		11.86	11.9	11.9

Storage Tanks Controlled Emissions (TANKS Output)	Tank 1	Tank 2	Tank 3	Proposed Permit Annual Emissions	Proposed Permit Hourly Emissions	58.01.01 Screening Level
Air Pollutant	Ibs/yr	Ibs/yr	Ibs/yr	Ibs/yr	Ibs/hr	Ibs/hr
Benzene	0.17	0.36	0.25	0.78	8.90E-05	8.00E-04
Ethylbenzene	0.08	0.17	0.12	0.37	4.22E-05	29
Naphthalene	0.00	0.00	0.00	0.00	0.00E+00	3.33
Tetrachloroethene	0.10	0.22	0.16	0.48	5.48E-05	1.30E-02
Toluene	0.99	2.12	1.51	4.62	5.27E-04	25
1,2,4-Trimethylbenzene	0.07	0.15	0.11	0.33	3.77E-05	8.2
Xylenes	0.44	0.95	0.68	2.07	2.36E-04	29
Fuel Oil VOCs	0.21	0.46	0.32	0.99	1.13E-04	--

Table 3: Processing Tanks 5-8 Estimated Emissions

TANKS Input Data		Tank 5	Tank 6	Tank 7	Tank 8
Tank Type		Horizontal Heated			
Tank Contents		Used Oil			
Tank Exterior		Orange Insulation ("Red")	Silver Paint	Rust ("Red")	
Tank Length (ft)	32.3	32.3	25.0	29.5	
Tank Diameter (ft)	8.3	8.3	9.2	7.8	
	12929	12929	12341	10544	
Tank Working Vol (gals)	10,500	10,500	10,000	8,500	
Max / Annual Operations	Batches/yr	365	365	365	365
Calcd Thruput (gal)		3,832,500	3,832,500	3,650,000	3,102,500
					Total (gal) 14,417,500

Processing Tanks Uncontrolled Emissions (TANKS Output)		Tank 5	Tank 6	Tank 7	Tank 8	Unrestricted Annual Emissions	Unrestricted Hourly Emissions	Impact at 1 lb/hr Emissions	Persistence Factor	Impact at Actual AAC/AACC Rate	58.01.01 Impact, % of AAC/AACC
Air Pollutant	lbs/yr	lbs/batch	lbs/yr	lbs/batch	lbs/yr	lbs/yr	lbs/hr	ug/m <sup>3</sup>	ug/m <sup>3</sup>	ug/m <sup>3</sup>	%
Benzene	3.58	0.0098	3.58	0.0098	3.41	0.0093	2.91	0.0080	13.48	0.125	137.2%
Ethylbenzene	1.03	0.0028	1.03	0.0028	0.99	0.0027	0.84	0.0023	3.89	0.16	0.12
Naphthalene	0.04	0.0001	0.04	0.0001	0.04	0.0001	0.03	0.0001	0.15	0.4	0.15
Tetrachloroethene	1.72	0.0047	1.72	0.0047	1.64	0.0045	1.40	0.0038	6.48	0.125	0.08
Toluene	17.99	0.0493	17.99	0.0493	17.15	0.0470	14.61	0.0400	67.74	7.73E-03	2.1
1,2,4-Trimethylbenzene	1.53	0.0042	1.53	0.0042	1.46	0.0040	1.24	0.0034	5.76	6.58E-04	18.75
Xylenes	7.22	0.0198	7.22	0.0198	6.98	0.0191	5.86	0.0161	27.28	8.2	14.1%
Fuel Oil VOCs	0.03	0.0001	0.03	0.0001	0.03	0.0001	0.03	0.0001	0.12	3.11E-03	6.15
											3.7%
											4.9%
											—
											—

Proposed Operations		Tank 5	Tank 6	Tank 7	Tank 8
Permitted Throughput (gal/yr)	Total		3,500,000		
Per Tank	1,400,000	1,400,000	350,000	350,000	
Batches per Year	133.3	133.3	35.0	35.0	41.2

Processing Tanks Controlled Emissions		Tank 5	Tank 6	Tank 7	Tank 8	Proposed Permit Annual Emissions	Proposed Permit Hourly Emissions
Air Pollutant	lbs/yr	lbs/yr	lbs/yr	lbs/yr	lbs/yr	lbs/hr	lbs/hr
Benzene	1.3078	1.3078	0.3270	0.3283	3.27	4.62E-04	
Ethylbenzene	0.3763	0.3763	0.0949	0.0948	0.94	1.08E-04	
Naphthalene	0.0146	0.0146	0.0038	0.0034	0.04	4.16E-06	
Tetrachloroethene	0.6283	0.6283	0.1573	0.1579	1.57	1.79E-04	
Toluene	6.5717	6.5717	1.6445	1.6482	16.44	1.88E-03	
1,2,4-Trimethylbenzene	0.5589	—	0.1400	0.1599	1.40	1.60E-04	
Xylenes	2.6374	2.6374	0.6693	0.6611	6.61	7.54E-04	
Fuel Oil VOCs	0.0110	0.0110	0.0029	0.0034	0.03	3.22E-06	

**Table 4: Proposed Facility-Wide Emissions  
of Criteria and Toxic Air Pollutants**

Criteria Pollutants - Facility Total	Averaging Period	Modeling Threshold (ton/yr)	Unrestricted Boiler Emissions (ton/yr)	Proposed Storage Tanks 1-3 Emissions (ton/yr)	Proposed Process Tanks 5-8 Emissions (ton/yr)	Proposed Combined Emissions (ton/yr)
NO <sub>x</sub>	Annual	1.0	2.74	--	--	2.74
VOC	Annual	--	0.16	0.005	0.015	0.18

Toxic Air Pollutants - Facility Total	TAP Type (24 hr or Annual Averaging)	58.01.01 Screening Emission Level (lb/hr)	Unrestricted Boiler Emissions (lb/hr)	Proposed Storage Tanks 1-3 Emissions (lb/hr)	Proposed Process Tanks 5-8 Emissions (lb/hr)	Proposed Combined Emissions (lb/hr)	Proposed Combined Emissions (% of EL)
Arsenic	586 (Annual)	1.50E-06	1.33E-06			1.33E-06	88.9%
Barium	585 (24 hr)	0.033	2.93E-05			2.93E-05	0.09%
Benzene	586 (Annual)	8.00E-04	1.40E-05	8.90E-05	4.62E-04	5.65E-04	70.7%
Cadmium	586 (Annual)	3.70E-06	7.33E-06			7.33E-06	198.2%
Chromium	585 (24 hr)	0.033	9.33E-06			9.33E-06	0.03%
Cobalt	585 (24 hr)	0.0070	5.60E-07			5.60E-07	0.01%
Copper	585 (24 hr)	0.07	5.67E-06			5.67E-06	0.01%
Dichlorobenzene	585 (24 hr)	20	8.00E-06			8.00E-06	0.00004%
Ethyl Benzene	585 (24 hr)	29		4.22E-05	1.08E-04	1.50E-04	0.0005%
Formaldehyde	586 (Annual)	5.10E-04	5.00E-04			5.00E-04	98.0%
n-Hexane	585 (24 hr)	12	1.20E-02			1.20E-02	0.10%
Manganese	585 (24 hr)	0.060	2.53E-06			2.53E-06	0.004%
Mercury	585 (24 hr)	0.001	1.73E-06			1.73E-06	0.17%
Molybdenum	585 (24 hr)	0.333	7.33E-06			7.33E-06	0.002%
Naphthalene	585 (24 hr)	3.33	4.07E-06	0.00E+00	4.16E-06	8.23E-06	0.0002%
Nickel	586 (Annual)	2.70E-05	1.40E-05			1.40E-05	51.9%
Pentane	585 (24 hr)	118	1.73E-02			1.73E-02	0.01%
Tetrachloroethene	586 (Annual)	1.30E-02		5.48E-05	1.79E-04	2.34E-04	1.8%
Toluene	585 (24 hr)	25	2.27E-05	5.27E-04	1.88E-03	2.43E-03	0.01%
1,2,4 Trimethylbenzene	585 (24 hr)	8.2		3.77E-05	1.60E-04	1.97E-04	0.002%
Vanadium	585 (24 hr)	0.003	1.53E-05			1.53E-05	0.51%
Xylenes	585 (24 hr)	29		2.36E-04	7.54E-04	9.90E-04	0.003%
Zinc	585 (24 hr)	0.067	1.93E-04			1.93E-04	0.29%

Modeling Protocol  
Commercial Fuel, Nampa, Idaho  
October 31, 2007

Appendix A:  
TANKS Run Reports  
(only input and report summary pages included)

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

User Identification:	Tank 1 RFOP
City:	Boise
State:	Idaho
Company:	Commercial Fuel
Type of Tank:	Vertical Fixed Roof Tank
Description:	Recycled Fuel Oil Product VFixedRT

**Tank Dimensions**

Shell Height (ft):	24.00
Diameter (ft):	22.90
Liquid Height (ft) :	19.50
Avg. Liquid Height (ft):	12.00
Volume (gallons):	60,000.00
Turnovers:	11.86
Net Throughput(gal/yr):	711,600.00
Is Tank Heated (y/n):	N

**Paint Characteristics**

Shell Color/Shade:	White/White
Shell Condition	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

**Roof Characteristics**

Type:	Dome
Height (ft)	0.00
Radius (ft) (Dome Roof)	0.00

**Breather Vent Settings**

Vacuum Settings (psig):	0.00
Pressure Settings (psig)	0.00

Meteorological Data used in Emissions Calculations: Boise, Idaho (Avg Atmospheric Pressure = 13.28 psia)

Tank #1

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Liquid Contents of Storage Tank**

**Tank 1 RFOP - Vertical Fixed Roof Tank****Boise, Idaho**

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg F)			Liquid Bulk Temp (deg F)	Vapor Pressure (psia)			Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
		Avg.	Min.	Max.		Avg.	Min.	Max.					
Recycled Fuel Oil Product	All	52.81	46.88	58.74	50.94	0.0006	0.0005	0.0007	102.6496			385.71	
1,2,4-Trimethylbenzene						0.0152	0.0119	0.0194	120.1900	0.0003	0.0333	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9535	0.8024	1.1277	78.1100	0.0000	0.0804	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0841	0.0677	0.1039	106.1700	0.0001	0.0389	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Naphthalene						0.0018	0.0014	0.0023	128.2000	0.0001	0.0006	128.20	Option 2: A=7.3729, B=1968.36, C=222.61
Residual oil no. 6						0.0000	0.0000	0.0000	190.0000	0.9987	0.1028	387.00	Option 1: VP50 = .00003 VP60 = .00004
Tetrachloroethylene						0.1631	0.1331	0.1987	165.8300	0.0000	0.0507	165.83	Option 2: A=6.98, B=1386.92, C=217.53
Toluene						0.2629	0.2166	0.3174	92.1300	0.0003	0.4789	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Xylenes (mixed isomers)						0.0699	0.0561	0.0865	106.1700	0.0005	0.2144	106.17	Option 2: A=7.009, B=1462.266, C=215.11

Tank #1

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Tank 1 RFOP - Vertical Fixed Roof Tank**  
**Boise, Idaho**

Components	Losses(lbs)		
	Working Loss	Breathing Loss	Total Emissions
Recycled Fuel Oil Product	1.02	1.04	2.06
Benzene	0.08	0.08	0.17
Ethylbenzene	0.04	0.04	0.08
Naphthalene	0.00	0.00	0.00
Tetrachloroethylene	0.05	0.05	0.10
Toluene	0.49	0.50	0.99
1,2,4-Trimethylbenzene	0.03	0.03	0.07
Residual oil no. 6	0.11	0.11	0.21
Xylenes (mixed isomers)	0.22	0.22	0.44

Tank #1

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

User Identification: Tank 2 RFOP  
City: Boise  
State: Idaho  
Company: Commercial Fuel  
Type of Tank: Vertical Fixed Roof Tank  
Description: Recycled Fuel Oil Product VFixedRT

**Tank Dimensions**

Shell Height (ft):	28.30
Diameter (ft):	29.95
Liquid Height (ft) :	25.50
Avg. Liquid Height (ft):	14.00
Volume (gallons):	135,000.00
Turnovers:	11.86
Net Throughput(gal/yr):	1,601,100.00
Is Tank Heated (y/n):	N

**Paint Characteristics**

Shell Color/Shade: White/White  
Shell Condition: Good  
Roof Color/Shade: White/White  
Roof Condition: Good

**Roof Characteristics**

Type:	Dome
Height (ft)	0.00
Radius (ft) (Dome Roof)	0.00

**Breather Vent Settings**

Vacuum Settings (psig):	0.00
Pressure Settings (psig)	0.00

Meteorological Data used in Emissions Calculations: Boise, Idaho (Avg Atmospheric Pressure = 13.28 psia)

Tank #2

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Liquid Contents of Storage Tank**

**Tank 2 RFOP - Vertical Fixed Roof Tank**  
**Boise, Idaho**

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg F)			Liquid Bulk Temp (deg F)	Vapor Pressure (psia)			Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
		Avg.	Min.	Max.		Avg.	Min.	Max.					
Recycled Fuel Oil Product	All	52.81	46.88	58.74	50.94	0.0006	0.0005	0.0007	102.6496			385.71	
1,2,4-Trimethylbenzene						0.0152	0.0119	0.0194	120.1900	0.0003	0.0333	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9535	0.8024	1.1277	78.1100	0.0000	0.0804	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0841	0.0677	0.1039	106.1700	0.0001	0.0389	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Naphthalene						0.0018	0.0014	0.0023	128.2000	0.0001	0.0006	128.20	Option 2: A=7.3729, B=1968.36, C=222.61
Residual oil no. 6						0.0000	0.0000	0.0000	190.0000	0.9987	0.1028	387.00	Option 1: VP50 = .00003 VP60 = .00004
Tetrachloroethylene						0.1631	0.1331	0.1987	165.8300	0.0000	0.0507	165.83	Option 2: A=6.98, B=1386.92, C=217.53
Toluene						0.2629	0.2166	0.3174	92.1300	0.0003	0.4789	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Xylenes (mixed isomers)						0.0699	0.0561	0.0865	106.1700	0.0005	0.2144	106.17	Option 2: A=7.009, B=1462.266, C=215.11

Tank #2

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Tank 2 RFOP - Vertical Fixed Roof Tank**  
**Boise, Idaho**

Components	Losses(lbs)		
	Working Loss	Breathing Loss	Total Emissions
Recycled Fuel Oil Product	2.30	2.14	4.44
Benzene	0.19	0.17	0.36
Ethylbenzene	0.09	0.08	0.17
Naphthalene	0.00	0.00	0.00
Tetrachloroethylene	0.12	0.11	0.22
Toluene	1.10	1.02	2.12
1,2,4-Trimethylbenzene	0.08	0.07	0.15
Residual oil no. 6	0.24	0.22	0.46
Xylenes (mixed isomers)	0.49	0.46	0.95

Tank #2

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

User Identification: Tank 3 RFOP  
City: Boise  
State: Idaho  
Company: Commercial Fuel  
Type of Tank: Vertical Fixed Roof Tank  
Description: Recycled Fuel Oil Product VFixedRT

**Tank Dimensions**

Shell Height (ft):	20.10
Diameter (ft):	30.00
Liquid Height (ft) :	18.00
Avg. Liquid Height (ft):	10.00
Volume (gallons):	100,000.00
Turnovers:	11.86
Net Throughput(gal/yr):	1,186,000.00
Is Tank Heated (y/n):	N

**Paint Characteristics**

Shell Color/Shade: White/White  
Shell Condition: Good  
Roof Color/Shade: White/White  
Roof Condition: Good

**Roof Characteristics**

Type:	Cone
Height (ft)	3.00
Slope (ft/ft) (Cone Roof)	0.10

**Breather Vent Settings**

Vacuum Settings (psig):	0.00
Pressure Settings (psig)	0.00

Meteorological Data used in Emissions Calculations: Boise, Idaho (Avg Atmospheric Pressure = 13.28 psia)

Tank #3

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Liquid Contents of Storage Tank**

**Tank 3 RFOP - Vertical Fixed Roof Tank**  
**Boise, Idaho**

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg F)			Liquid Bulk Temp (deg F)	Vapor Pressure (psia)			Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
		Avg.	Min.	Max.		Avg.	Min.	Max.					
Recycled Fuel Oil Product	All	52.81	46.88	58.74	50.94	0.0006	0.0005	0.0007	102.6496			385.71	
1,2,4-Trimethylbenzene						0.0152	0.0119	0.0194	120.1900	0.0003	0.0333	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						0.9535	0.8024	1.1277	78.1100	0.0000	0.0804	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						0.0841	0.0677	0.1039	106.1700	0.0001	0.0389	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Naphthalene						0.0018	0.0014	0.0023	128.2000	0.0001	0.0006	128.20	Option 2: A=7.3729, B=1968.36, C=222.61
Residual oil no. 6						0.0000	0.0000	0.0000	190.0000	0.9987	0.1028	387.00	Option 1: VP50 = .00003 VP60 = .00004
Tetrachloroethylene						0.1631	0.1331	0.1987	165.8300	0.0000	0.0507	165.83	Option 2: A=6.98, B=1386.92, C=217.53
Toluene						0.2629	0.2166	0.3174	92.1300	0.0003	0.4789	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Xylenes (mixed isomers)						0.0699	0.0561	0.0865	106.1700	0.0005	0.2144	106.17	Option 2: A=7.009, B=1462.266, C=215.11

Tank #3

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Tank 3 RFOP - Vertical Fixed Roof Tank**  
**Boise, Idaho**

Components	Losses(lbs)		
	Working Loss	Breathing Loss	Total Emissions
Recycled Fuel Oil Product	1.70	1.45	3.16
Benzene	0.14	0.12	0.25
Ethylbenzene	0.07	0.06	0.12
Naphthalene	0.00	0.00	0.00
Tetrachloroethylene	0.09	0.07	0.16
Toluene	0.82	0.70	1.51
1,2,4-Trimethylbenzene	0.06	0.05	0.11
Residual oil no. 6	0.18	0.15	0.32
Xylenes (mixed isomers)	0.37	0.31	0.68

Tank #3

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

User Identification: Tank 5 Daily Batch  
City: Boise  
State: Idaho  
Company: Commercial Fuel  
Type of Tank: Horizontal Tank  
Description: Heated Hor Processing Tank

**Tank Dimensions**

Shell Length (ft):	32.33
Diameter (ft):	8.25
Volume (gallons):	10,500.00
Turnovers:	365.00
Net Throughput(gal/yr):	3,832,500.00
Is Tank Heated (y/n):	Y
Is Tank Underground (y/n):	N

**Paint Characteristics**

Shell Color/Shade: Red/Primer  
Shell Condition: Good

**Breather Vent Settings**

Vacuum Settings (psig):	0.00
Pressure Settings (psig)	0.00

Meteorological Data used in Emissions Calculations: Boise, Idaho (Avg Atmospheric Pressure = 13.28 psia)

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Liquid Contents of Storage Tank**

**Tank 5 Daily Batch - Horizontal Tank**  
**Boise, Idaho**

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg F)				Liquid Bulk Temp (deg F)	Vapor Pressure (psia)			Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
		Avg.	Min.	Max.	(deg F)		Avg.	Min.	Max.					
Used Oil Feed	All	140.00	60.00	220.00	220.00	0.0087	0.0010	0.0415	96.7942		0.0003	0.0461	385.48	Option 2: A=7.04383, B=1573.267, C=208.56
1,2,4-Trimethylbenzene						0.2965	0.0204	2.0131	120.1900		0.0000	0.1081	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Benzene						7.5585	1.1679	29.3641	78.1100		0.0000	0.0312	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Ethylbenzene						1.1177	0.1085	5.9941	106.1700		0.0001	0.0012	128.20	Option 2: A=7.3729, B=1968.36, C=222.61
Naphthalene						0.0495	0.0025	0.4374	128.2000		0.9985	0.0010	387.00	Option 3: A=83897.34, B=-9.503
Residual Fuel Oil No. 6 above 100 F						0.0000	0.0000	0.0002	190.0000		0.0518	0.0518	165.83	Option 2: A=6.98, B=1386.92, C=217.53
Tetrachloroethylene						1.8579	0.2071	9.0958	165.8300		0.0001	0.5427	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Toluene						2.6828	0.3301	12.2687	92.1300		0.0004	0.2179	106.17	Option 2: A=7.009, B=1462.266, C=215.11
Xylenes (mixed isomers)						0.9554	0.0904	5.2412	106.1700		0.0005			

**Emissions Report - Detail Format  
Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Tank 5 Daily Batch - Horizontal Tank  
Boise, Idaho**

Components	Losses(lbs)		
	Working Loss	Breathing Loss	Total Emissions
Used Oil Feed	19.04	14.10	33.14
Benzene	2.06	1.52	3.58
Ethylbenzene	0.59	0.44	1.03
Naphthalene	0.02	0.02	0.04
Tetrachloroethylene	0.99	0.73	1.72
Toluene	10.33	7.65	17.99
1,2,4-Trimethylbenzene	0.88	0.65	1.53
Xylenes (mixed isomers)	4.15	3.07	7.22
Residual Fuel Oil No. 6 above 100 F	0.02	0.01	0.03

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

User Identification:	Tank 7 Used Oil
City:	Boise
State:	Idaho
Company:	Commercial Fuel
Type of Tank:	Horizontal Tank
Description:	Heated Hor Processing Tank

**Tank Dimensions**

Shell Length (ft):	25.00
Diameter (ft):	9.17
Volume (gallons):	10,000.00
Turnovers:	365.00
Net Throughput(gal/yr):	3,650,000.00
Is Tank Heated (y/n):	Y
Is Tank Underground (y/n):	N

**Paint Characteristics**

Shell Color/Shade:	White/White
Shell Condition	Good

**Breather Vent Settings**

Vacuum Settings (psig):	0.00
Pressure Settings (psig)	0.00

Meteorological Data used in Emissions Calculations: Boise, Idaho (Avg Atmospheric Pressure = 13.28 psia)

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Liquid Contents of Storage Tank**

**Tank 7 Used Oil - Horizontal Tank**  
**Boise, Idaho**

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg F)			Liquid Bulk Temp (deg F)	Vapor Pressure (psia)			Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
		Avg.	Min.	Max.		Avg.	Min.	Max.					
Used Oil Feed	All	140.00	60.00	220.00	220.00	0.0087	0.0010	0.0415	96.7942			385.48	
1,2,4-Trimethylbenzene						0.2965	0.0204	2.0131	120.1900	0.0003	0.0461	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						7.5585	1.1679	29.3641	78.1100	0.0000	0.1081	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						1.1177	0.1085	5.9941	106.1700	0.0001	0.0312	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Naphthalene						0.0495	0.0025	0.4374	128.2000	0.0001	0.0012	128.20	Option 2: A=7.3729, B=1968.36, C=222.61
Residual Fuel Oil No. 6 above 100 F						0.0000	0.0000	0.0002	190.0000	0.9985	0.0010	387.00	Option 3: A=83897.34, B=9.503
Tetrachloroethylene						1.8579	0.2071	9.0958	165.8300	0.0001	0.0518	165.83	Option 2: A=6.98, B=1386.92, C=217.53
Toluene						2.6828	0.3301	12.2687	92.1300	0.0004	0.5427	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Xylenes (mixed isomers)						0.9554	0.0904	5.2412	106.1700	0.0005	0.2179	106.17	Option 2: A=7.009, B=1462.266, C=215.11

**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Tank 7 Used Oil - Horizontal Tank**

**Boise, Idaho**

Components	Losses(lbs)		
	Working Loss	Breathing Loss	Total Emissions
Used Oil Feed	18.13	13.46	31.59
Benzene	1.96	1.45	3.41
Ethylbenzene	0.57	0.42	0.99
Naphthalene	0.02	0.02	0.04
Tetrachloroethylene	0.94	0.70	1.64
Toluene	9.84	7.30	17.15
1,2,4-Trimethylbenzene	0.84	0.62	1.46
Xylenes (mixed isomers)	3.95	2.93	6.88
Residual Fuel Oil No. 6 above 100 F	0.02	0.01	0.03

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

User Identification: Tank 8 Used Oil  
City: Boise  
State: Idaho  
Company: Commercial Fuel  
Type of Tank: Horizontal Tank  
Description: Heated Hor Processing Tank

**Tank Dimensions**

Shell Length (ft):	29.50
Diameter (ft):	7.80
Volume (gallons):	8,500.00
Turnovers:	365.00
Net Throughput(gal/yr):	3,102,500.00
Is Tank Heated (y/n):	Y
Is Tank Underground (y/n):	N

**Paint Characteristics**

Shell Color/Shade: Red/Primer  
Shell Condition: Poor

**Breather Vent Settings**

Vacuum Settings (psig):	0.00
Pressure Settings (psig)	0.00

Meteorological Data used in Emissions Calculations: Boise, Idaho (Avg Atmospheric Pressure = 13.28 psia)

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Liquid Contents of Storage Tank**

**Tank 8 Used Oil - Horizontal Tank**  
**Boise, Idaho**

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg F)			Liquid Bulk Temp (deg F)	Vapor Pressure (psia)			Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
		Avg.	Min.	Max.		Avg.	Min.	Max.					
Used Oil Feed	All	140.00	60.00	220.00	220.00	0.0087	0.0010	0.0415	96.7942			385.48	
1,2,4-Trimethylbenzene						0.2965	0.0204	2.0131	120.1900	0.0003	0.0461	120.19	Option 2: A=7.04383, B=1573.267, C=208.56
Benzene						7.5585	1.1679	29.3641	78.1100	0.0000	0.1081	78.11	Option 2: A=6.905, B=1211.033, C=220.79
Ethylbenzene						1.1177	0.1085	5.9941	106.1700	0.0001	0.0312	106.17	Option 2: A=6.975, B=1424.255, C=213.21
Naphthalene						0.0495	0.0025	0.4374	128.2000	0.0001	0.0012	128.20	Option 2: A=7.3729, B=1968.36, C=222.61
Residual Fuel Oil No. 6 above 100 F						0.0000	0.0000	0.0002	190.0000	0.9985	0.0010	387.00	Option 3: A=83897.34, B=9.503
Tetrachloroethylene						1.8579	0.2071	9.0958	165.8300	0.0001	0.0518	165.83	Option 2: A=6.98, B=1386.92, C=217.53
Toluene						2.6828	0.3301	12.2687	92.1300	0.0004	0.5427	92.13	Option 2: A=6.954, B=1344.8, C=219.48
Xylenes (mixed isomers)						0.9554	0.0904	5.2412	106.1700	0.0005	0.2179	106.17	Option 2: A=7.009, B=1462.266, C=215.11

**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Tank 8 Used Oil - Horizontal Tank**  
**Boise, Idaho**

Components	Losses(lbs)		
	Working Loss	Breathing Loss	Total Emissions
Used Oil Feed	15.41	11.50	26.91
Benzene	1.67	1.24	2.91
Ethylbenzene	0.48	0.36	0.84
Naphthalene	0.02	0.01	0.03
Tetrachloroethylene	0.80	0.60	1.40
Toluene	8.36	6.24	14.61
1,2,4-Trimethylbenzene	0.71	0.53	1.24
Xylenes (mixed isomers)	3.36	2.51	5.86
Residual Fuel Oil No. 6 above 100 F	0.02	0.01	0.03

**Modeling Protocol**  
**Commercial Fuel, Nampa, Idaho**  
**October 31, 2007**

**Appendix B;**  
**Used Oil and Recycled Fuel Oil Product Analytical Results**

# Anatek Labs, Inc.

1282 Alturas Drive • Moscow, ID 83843 • (208) 883-2839 • Fax (208) 882-9246 • email moscow@anateklabs.com  
504 E Sprague Ste. D • Spokane WA 99202 • (509) 838-3999 • Fax (509) 838-4433 • email spokane@anateklabs.com

**Client:** COMMERCIAL FUEL RECYCLING      **Batch #:** 070420023  
**Address:** 7336 CORAL CT      **Project Name:** PROCESS COMPARISONS  
NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

## Analytical Results Report

Sample Number	070420023-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 UNPROCESSED					
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
1,1,1,2-Tetrachloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1,1-Trichloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1,2,2-Tetrachloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1,2-Trichloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1-Dichloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1-Dichloroethene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1-dichloropropene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2,3-Trichloropropane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2,4-Trimethylbenzene	338	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2-Dibromoethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2-Dichlorobenzene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2-Dichloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2-Dichloropropane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,3-Dichlorobenzene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,3-Dichloropropane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,4-Dichlorobenzene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
2,2-Dichloropropane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
2-hexanone	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Acetone	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Benzene	31.1	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Bromochloromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Bromodichloromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Bromoform	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Carbon Tetrachloride	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Chlorobenzene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Chloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Chloroform	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Chloromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
cis-1,2-dichloroethene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
cis-1,3-Dichloropropene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Dibromochloromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Dibromomethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Dichlorodifluoromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Ethylbenzene	60.7	mg/kg	10	4/30/2007	TGT	EPA 8260B	

**Comments:**

# Anatek Labs, Inc.

Used Oil Feed  
Page 2 of 7

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**Client:** COMMERCIAL FUEL RECYCLING  
**Address:** 7336 CORAL CT  
 NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

**Batch #:** 070420023  
**Project Name:** PROCESS COMPARISONS

## Analytical Results Report

Sample Number	070420023-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 UNPROCESSED					
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
Hexachlorobutadiene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
m+p-Xylene	86.9	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Methyl ethyl ketone (MEK)	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Methyl isobutyl ketone (MIBK)	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Methylene chloride	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
methyl-t-butyl ether (MTBE)	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Naphthalene	46.2	mg/kg	10	4/30/2007	TGT	EPA 8260B	
o-Xylene	409	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Styrene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Tetrachloroethene	60.7	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Toluene	440	mg/kg	10	4/30/2007	TGT	EPA 8260B	
trans-1,2-Dichloroethene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
trans-1,3-Dichloropropene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Trichloroethene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Trichlorofluoromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Vinyl Chloride	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	

## Surrogate Data

Sample Number	070420023-001	Method	Percent Recovery	Control Limits
Surrogate Standard				
1,2-Dichlorobenzene-d4	EPA 8260B	98.0	70-130	
4-Bromofluorobenzene	EPA 8260B	100.8	70-130	
Toluene-d8	EPA 8260B	104.0	70-130	

Authorized Signature

MCL      EPA's Maximum Contaminant Level  
 ND      Not Detected  
 PQL     Practical Quantitation Limit

## Comments:

Tuesday, May 08, 2007

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# Anatek Labs, Inc.

1282 Alturas Drive • Moscow, ID 83843 • (208) 883-2839 • Fax (208) 882-9246 • email moscow@anateklabs.com  
504 E Sprague Ste. D • Spokane WA 99202 • (509) 838-3999 • Fax (509) 838-4433 • email spokane@anateklabs.com

**Client:** COMMERCIAL FUEL RECYCLING  
**Address:** 7336 CORAL CT  
NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

**Batch #:** 070420023  
**Project Name:** PROCESS COMPARISONS

## Analytical Results Report

Sample Number	070420023-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 UNPROCESSED			Extraction Date	5/3/2007	
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
1,2,4-Trichlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1,2-Dichlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1,2-Diphenyl hydrazine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1,3-Dichlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1,4-Dichlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1-Methylnaphthalene	69.1	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,3,4,6-Tetrachlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,3,5,6-Tetrachlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4,5-Trichlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4,6-Trichlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4-Dichlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4-Dimethylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4-Dinitrophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4-Dinitrotoluene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,6-Dinitrotoluene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Chloronaphthalene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Chlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Methylnaphthalene	114	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Methylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Nitroaniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Nitrophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
3,3'-Dichlorobenzidine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
3+4-Methylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
3-Nitroaniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4,6-Dinitro-2-methylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Bromophenyl-phenylether	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Chloro-3-methylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Chloroaniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Chlorophenyl-phenylether	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Nitroaniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Nitrophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Acenaphthene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Acenaphthylene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Aniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	

**Comments:**

Tuesday, May 08, 2007

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Used Oil Feed  
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**Client:** COMMERCIAL FUEL RECYCLING  
**Address:** 7336 CORAL CT  
 NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

**Batch #:** 070420023  
**Project Name:** PROCESS COMPARISONS

## Analytical Results Report

Sample Number	070420023-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 UNPROCESSED			Extraction Date	5/3/2007	
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
Anthracene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzidine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo(ghi)perylene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo[a]anthracene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo[a]pyrene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo[b]fluoranthene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo[k]fluoranthene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzyl alcohol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
bis(2-Chloroethoxy)methane	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
bis(2-Chloroethyl)ether	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
bis(2-chloroisopropyl)ether	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
bis(2-Ethylhexyl)phthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Butylbenzylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Carbazole	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Chrysene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Dibenz[a,h]anthracene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Dibenzofuran	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Diethylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Dimethylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Di-n-butylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Di-n-octylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Fluoranthene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Fluorene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Hexachlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Hexachlorobutadiene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Hexachlorocyclopentadiene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Hexachloroethane	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Indeno[1,2,3-cd]pyrene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Isophorone	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Naphthalene	53.9	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Nitrobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Nitrosodimethylamine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
n-Nitroso-di-n-propylamine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
n-Nitrosodiphenylamine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Pentachlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Phenanthrene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	

**Comments:**

Tuesday, May 08, 2007

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**Client:** COMMERCIAL FUEL RECYCLING  
**Address:** 7336 CORAL CT  
NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

**Batch #:** 070420023  
**Project Name:** PROCESS COMPARISONS

## Analytical Results Report

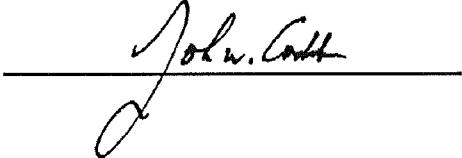
Sample Number	070420023-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 UNPROCESSED			Extraction Date	5/3/2007	
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
Phenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Pyrene	14.4	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Pyridine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	

## Surrogate Data

Sample Number	070420023-001	Surrogate Standard	Method	Percent Recovery	Control Limits
		2,4,6-Tribromophenol	EPA 8270C	89.3	19-125
		2-Fluorobiphenyl	EPA 8270C	89.2	30-125
		2-Fluorophenol	EPA 8270C	83.7	25-130
		Nitrobenzene-d5	EPA 8270C	88.0	23-120
		Phenol-d5	EPA 8270C	81.5	24-125
		Terphenyl-d14	EPA 8270C	100.0	18-140

Authorized Signature



MCL EPA's Maximum Contaminant Level  
ND Not Detected  
PQL Practical Quantitation Limit

## Comments:

Tuesday, May 08, 2007

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1282 Alturas Dr Moscow ID 83843 (208) 883-2839 FAX 882-9246  
moscow@anateklabs.com

May 8, 2007

**Commercial Fuel Recycling**  
7336 Coral Ct  
Nampa ID, 83687  
Project Manager: Mark Desrosiers

Laboratory Project #: 070420023  
Customer Project: 041807 Unprocessed - Process Comparisons  
Date Received: 4/20/07

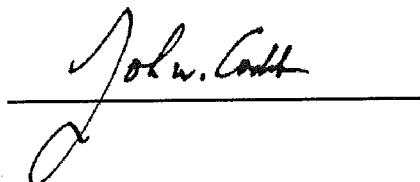
EDL = Estimated Detection Limit

**Sample ID: 041807 Unprocessed**

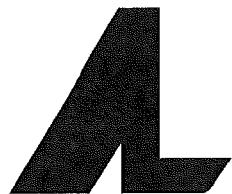
Analyte	Method	Result	EDL	Units	Analysis Date	Analyst
TOX	EPA 9076	199	100	mg/Kg	4/25/2007	WOZ
PCB 1242	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1254	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1232	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1260	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1248	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1016	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1221	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
Flashpoint	EPA 1010	>200	N/A	Deg F	4/24/2007	SAT
Total Sulfur	D2622	0.33	0.01	%	5/1/2007	SAT
Ash	D2974	0.87	0.01	%	4/25/2007	SAT
Specific Gr.	D792	0.89	N/A		5/1/2007	JWC
BTU (BTU/lb)	D240	18400	10	BTU/lb	4/30/2007	JKL
BTU (BTU/gallon)	D240	138000	10	BTU/gal	4/30/2007	JKL
Total Glycol	EPA 8015mod	1060	100	mg/Kg	5/1/2007	EMP
Water	D95	3.5	0.01	%	5/1/2007	TOT*
BS&W	D1796	2.0	N/A	% vol	5/1/2007	TOT*

\* Analyzed by Texas Oil Tech Labs, Houston Texas

Approved by:



A handwritten signature in black ink, appearing to read "John Cott". It is positioned above a solid horizontal line. Below the line, there is a faint, stylized, cursive signature that looks like a 'J' or a 'C'.



# Anatek Labs, Inc.

1282 Alturas Drive • Moscow, ID 83843  
(208) 883-2839 • FAX 882-9246

[moscow@anateklabs.com](mailto:moscow@anateklabs.com)

Used Oil Feed  
Page 7 of 7

504 E Sprague Ste D • Spokane WA 99202  
(509) 838-3999 • FAX 838-4499

[www.anateklabs.com](http://www.anateklabs.com) [spokane@anateklabs.com](mailto:spokane@anateklabs.com)

May 9, 2007

Mark Desrosiers  
**Commercial Fuel Recycling**  
7336 Coral Ct  
Nampa, ID 83687

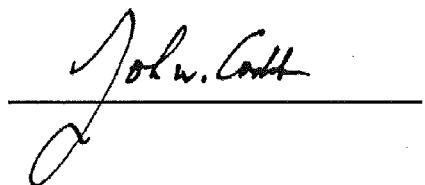
## Case Summary

TPH Fingerprint of Processed and Unprocessed Fuel Oil

Project Name: Process Comparisons  
Date Sampled: N/A  
Date Analyzed: 5/2/07  
Analyst: SAT

**Case Narrative** – Two oil samples were received on 4/20/2007 with proper chain of custody and in good condition. The two samples were labeled “041807 Processed” and “041807 Unprocessed” and were assigned Anatek Lab Sample ID’s 070420025-001 and 070420023-001 respectively. Each sample was diluted 1:500 in methylene chloride and injected onto an Agilent 6980n GC/FID. The sample chromatograms were compared to each other and to a retention time standard containing 14 n-hydrocarbons from C8 through C36. When the sample chromatograms were compared, they were determined to be identical. Comparison with TPH calibrations and the retention time standard indicate the samples contained negligible C6-C9 volatile hydrocarbons, >97% C22-C32 oil range hydrocarbons, and a small but finite amount of diesel range material (~3%).

Approved by:

  
John. Cott

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1282 Alturas Drive • Moscow, ID 83843 • (208) 883-2839 • Fax (208) 882-9246 • email moscow@anateklabs.com  
504 E Sprague Ste. D • Spokane WA 99202 • (509) 838-3999 • Fax (509) 838-4433 • email spokane@anateklabs.com

**Client:** COMMERCIAL FUEL RECYCLING  
**Address:** 7336 CORAL CT  
NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

**Batch #:** 070420025  
**Project Name:** PROCESS COMPARISONS

## Analytical Results Report

Sample Number	070420025-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 PROCESSED					
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
1,1,1,2-Tetrachloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1,1-Trichloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1,2,2-Tetrachloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1,2-Trichloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1-Dichloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1-Dichloroethene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,1-dichloropropene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2,3-Trichloropropane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2,4-Trimethylbenzene	342	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2-Dibromoethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2-Dichlorobenzene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2-Dichloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,2-Dichloropropane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,3-Dichlorobenzene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,3-Dichloropropane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
1,4-Dichlorobenzene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
2,2-Dichloropropane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
2-hexanone	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Acetone	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Benzene	13.2	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Bromochloromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Bromodichloromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Bromoform	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Carbon Tetrachloride	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Chlorobenzene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Chloroethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Chloroform	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Chloromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
cis-1,2-dichloroethene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
cis-1,3-Dichloropropene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Dibromochloromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Dibromomethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Dichlorodifluoromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Ethylbenzene	72.3	mg/kg	10	4/30/2007	TGT	EPA 8260B	

**Comments:**

# Anatek Labs, Inc.

Recycled Fuel Oil Product  
Page 2 of 6

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504 E Sprague Ste. D • Spokane WA 99202 • (509) 838-3999 • Fax (509) 838-4433 • email spokane@anateklabs.com

**Client:** COMMERCIAL FUEL RECYCLING  
**Address:** 7336 CORAL CT  
 NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

**Batch #:** 070420025  
**Project Name:** PROCESS COMPARISONS

## Analytical Results Report

Sample Number	070420025-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 PROCESSED					
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
Hexachlorobutadiene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
m+p-Xylene	343	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Methyl ethyl ketone (MEK)	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Methyl isobutyl ketone (MIBK)	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Methylene chloride	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
methyl-t-butyl ether (MTBE)	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Naphthalene	52.2	mg/kg	10	4/30/2007	TGT	EPA 8260B	
o-Xylene	137	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Styrene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Tetrachloroethene	48.6	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Toluene	285	mg/kg	10	4/30/2007	TGT	EPA 8260B	
trans-1,2-Dichloroethene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
trans-1,3-Dichloropropene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Trichloroethene	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Trichlorofluoromethane	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	
Vinyl Chloride	ND	mg/kg	10	4/30/2007	TGT	EPA 8260B	

## Surrogate Data

Sample Number	070420025-001	Surrogate Standard	Method	Percent Recovery	Control Limits
		1,2-Dichlorobenzene-d4	EPA 8260B	99.2	70-130
		4-Bromofluorobenzene	EPA 8260B	101.6	70-130
		Toluene-d8	EPA 8260B	103.6	70-130

Authorized Signature

MCL      EPA's Maximum Contaminant Level  
 ND      Not Detected  
 PQL      Practical Quantitation Limit

## Comments:

Tuesday, May 08, 2007

Page 2 of 2

# Anatek Labs, Inc.

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504 E Sprague Ste. D • Spokane WA 99202 • (509) 838-3999 • Fax (509) 838-4433 • email spokane@anateklabs.com

**Client:** COMMERCIAL FUEL RECYCLING  
**Address:** 7336 CORAL CT  
NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

**Batch #:** 070420025  
**Project Name:** PROCESS COMPARISONS

## Analytical Results Report

Sample Number	070420025-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 PROCESSED			Extraction Date	5/3/2007	
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
1,2,4-Trichlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1,2-Dichlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1,2-Diphenyl hydrazine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1,3-Dichlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1,4-Dichlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
1-Methylnaphthalene	68.3	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,3,4,6-Tetrachlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,3,5,6-Tetrachlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4,5-Trichlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4,6-Trichlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4-Dichlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4-Dimethylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4-Dinitrophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,4-Dinitrotoluene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2,6-Dinitrotoluene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Chloronaphthalene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Chlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Methylnaphthalene	105	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Methylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Nitroaniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
2-Nitrophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
3,3'-Dichlorobenzidine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
3+4-Methylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
3-Nitroaniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4,6-Dinitro-2-methylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Bromophenyl-phenylether	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Chloro-3-methylphenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Chloroaniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Chlorophenyl-phenylether	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Nitroaniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
4-Nitrophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Acenaphthene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Acenaphthylene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Aniline	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	

**Comments:**

# Anatek Labs, Inc.

Recycled Fuel Oil Product  
Page 4 of 6

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**Client:** COMMERCIAL FUEL RECYCLING  
**Address:** 7336 CORAL CT  
 NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

**Batch #:** 070420025  
**Project Name:** PROCESS COMPARISONS

## Analytical Results Report

Sample Number	070420025-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 PROCESSED			Extraction Date	5/3/2007	
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
Anthracene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzidine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo(ghi)perylene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo[a]anthracene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo[a]pyrene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo[b]fluoranthene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzo[k]fluoranthene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Benzyl alcohol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
bis(2-Chloroethoxy)methane	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
bis(2-Chloroethyl)ether	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
bis(2-chloroisopropyl)ether	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
bis(2-Ethylhexyl)phthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Butylbenzylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Carbazole	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Chrysene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Dibenz[a,h]anthracene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Dibenzofuran	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Diethylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Dimethylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Di-n-butylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Di-n-octylphthalate	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Fluoranthene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Fluorene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Hexachlorobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Hexachlorobutadiene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Hexachlorocyclopentadiene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Hexachloroethane	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Indeno[1,2,3-cd]pyrene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Isophorone	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Naphthalene	53.5	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Nitrobenzene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Nitrosodimethylamine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
n-Nitroso-di-n-propylamine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
n-Nitrosodiphenylamine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Pentachlorophenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Phenanthrene	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	

**Comments:**

Tuesday, May 08, 2007

Page 2 of 3

# Anatek Labs, Inc.

Recycled Fuel Oil Product  
Page 5 of 6

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504 E Sprague Ste. D • Spokane WA 99202 • (509) 838-3999 • Fax (509) 838-4433 • email spokane@anateklabs.com

**Client:** COMMERCIAL FUEL RECYCLING  
**Address:** 7336 CORAL CT  
NAMPA, ID 73687  
**Attn:** MARK DESROSIERS

**Batch #:** 070420025  
**Project Name:** PROCESS COMPARISONS

## Analytical Results Report

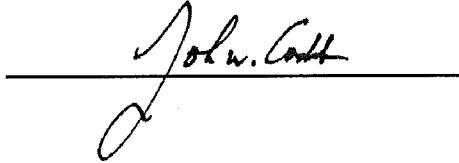
Sample Number	070420025-001	Sampling Date	4/18/2007	Date/Time Received	4/20/2007	11:10 AM
Client Sample ID	041807 PROCESSED			Extraction Date	5/3/2007	
Matrix:	Liquid					

Parameter	Result	Units	PQL	Analysis Date	Analyst	Method	Qualifier
Phenol	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Pyrene	16.3	mg/Kg	5	5/3/2007	EMP	EPA 8270C	
Pyridine	ND	mg/Kg	5	5/3/2007	EMP	EPA 8270C	

## Surrogate Data

Sample Number	070420025-001	Surrogate Standard	Method	Percent Recovery	Control Limits
		2,4,6-Tribromophenol	EPA 8270C	89.8	19-125
		2-Fluorobiphenyl	EPA 8270C	89.3	30-125
		2-Fluorophenol	EPA 8270C	78.9	25-130
		Nitrobenzene-d5	EPA 8270C	89.5	23-120
		Phenol-d5	EPA 8270C	78.6	24-125
		Terphenyl-d14	EPA 8270C	102.4	18-140

Authorized Signature



MCL      EPA's Maximum Contaminant Level  
ND      Not Detected  
PQL      Practical Quantitation Limit

## Comments:



May 8, 2007

**Commercial Fuel Recycling**

7336 Coral Ct

Nampa ID, 83687

Project Manager: Mark Desrosiers

Laboratory Project #: 070420025

Customer Project: 041807 Processed - Process Comparisons

Date Received: 4/20/07

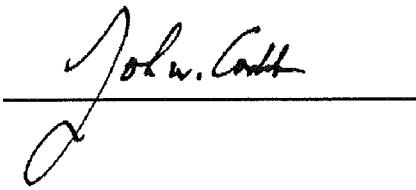
EDL = Estimated Detection Limit

**Sample ID: 041807 Processed**

Analyte	Method	Result	EDL	Units	Analysis Date	Analyst
TOX	EPA 9076	211	100	mg/Kg	4/25/2007	WOZ
PCB 1242	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1254	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1232	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1260	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1248	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1016	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
PCB 1221	EPA 8082	<1.0	1.0	mg/Kg	5/2/2007	ML
Flashpoint	EPA 1010	>200	N/A	Deg F	4/24/2007	SAT
Total Sulfur	D2622	0.33	0.01	%	5/1/2007	SAT
Ash	D2974	0.90	0.01	%	4/25/2007	SAT
Specific Gr.	D792	0.89	N/A		5/1/2007	JWC
BTU (BTU/lb)	D240	18400	10	BTU/lb	4/30/2007	JKL
BTU (BTU/gallon)	D240	138000	10	BTU/gal	4/30/2007	JKL
Total Glycol	EPA 8015mod	944	100	mg/Kg	5/1/2007	EMP
Water	D95	1.7	0.01	%	5/1/2007	TOT*
BS&W	D1796	2.0	N/A	% vol	5/1/2007	TOT*

\* Analyzed by Texas Oil Tech Labs, Houston Texas

Approved by:

  
John Cott